A CORRELATION OF ROTARY DRUM COOLER-FLAKER HEAT TRANSFER

K. L. Mai

Shell Chemical Corporation, Houston, Texas

Preprint 21

COPY 1

19961217 133

DTIC QUALITY INSPECTED

Presented at the

Second National Heat Transfer Conference

A.I.Ch.E.-A.S.M.E.

Chicago, Illinois

August 18 to 21, 1958

Copy No.

W

L

E   ①

A

H

ABSTRACT

A theoretical mathematical expression is presented
which effectively correlates rotary drum cooler-flaker design
and operating variables. Its application eliminates design
uncertainties introduced by the previous empirical approach,
and allows adjustment of operating variables for optimum
performance with a minimum of experimentation. The proposed
equation is derived from the general statement for unidirec-
tional unsteady state heat conduction in an infinite film
layer. The simplifications made in the derivation include the
assumption that the thermal properties of the liquid and
solid phases do not differ greatly and that the latent heat
of solidification averages in the sensible heat effect.

Extensive tests conducted with plant-size drum
cooler-flakers show experimental results to be in excellent
agreement with data predicted by the suggested expression.
Process stream exit temperatures correspond to within a
standard deviation of two percent (±3%) over wide ranges of
primary operating variables. It is felt that the results of
this work will prove to be of value in cooler-flaker sizing
and the choice of optimum operating conditions.

A CORRELATION OF ROTARY DRUM
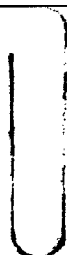
COOLER-FLAKER HEAT TRANSFER

INTRODUCTION

Rotary drum cooler-flakers are commonly used to
continuously cool, solidify, and flake melts. In recent
years they have widely displaced equivalent batch processing
equipment since they conserve processing time and working
space and eliminate the necessity of finished product crushing
and grinding prior to storage and shipment. The operation and
the construction of the flaking machines are so simple that
they can be applied to the processing of practically all
organic and inorganic chemical products that display a
definite melting point and possess a truly crystalline solid
structure at above ambient temperatures. The only limitation
placed on a more extensive application of rotary drum cooler-
flakers to materials meeting this melting point specification
is the lack of a firm design basis and the difficulty in
establishing optimum operating conditions. This has often
limited new installations to the processing of previously
tried systems.

- 1 -

Flaker sizing and design to date is largely based
on a backlog of processing information available to the
equipment manufacturers, and on extensive, time consuming
pilot plant tests. A complete empirical-statistical evalua-
tion of flaker performance is impractical due to the complex
inter-relationship of the numerous operating and design
variables and the inaccessibility of sufficient data taken
on a common basis. This work was therefore initiated with
the object of deriving a fundamental theoretical solution to
the rotary flaker heat transfer performance which would serve as
a springboard to a rational approach to flaker sizing and the
choice of optimum operating conditions. This paper covers the
method of mathematical analysis chosen and demonstrates the
excellent agreement of the results of this analysis with
available experimental data.

FLAKER OPERATION

The operation of rotary drum cooler flakers is
illustrated in the sketch of Figure 1. The flaker, or cooling
drum, is mounted on hollow tunnions which are set in bearings.
The drum dips to a depth, h, into a shallow pan filled with
the molten process material at temperature T_i. A variable speed

- 2 -

drive powers the drum which picks up a film of L M lb/hr of processing material. The film is cooled and solidified during film-drum contact time, b, and then scraped (flaked) from the drum surface by a doctor blade. The flake discharge temperature is T_o. The drum surface may be cooled by cooling water, a brine solution, or a refrigerant, sprayed on the inner drum periphery through manifolded nozzles. At high coolant rates with low coolant temperature drops the coolant temperature may be set at t, the arithmetic average of inlet and outlet temperatures t_i and t_o. The process film thickness is shown as R.

Primary and secondary operating variables are listed in Table I. The secondary variables are described as functions of the primary units. Of the primary operating variables the flake discharge temperature, T_o, is of greatest importance since product caking and sintering characteristics on transfer and storage are directly related to it. On the same basis this temperature usually limits the capacity of given size flaking units.

TABLE I

PRIMARY AND SECONDARY VARIABLES - FLAKER PROCESSING

Primary Variables:

T_o — Process Stream, Discharge Temperature, °F

T_i — Process Stream, Feed Temperature, °F

L — Processing Rate, M lb/hr

t_i — Cooling Water, Feed Temperature, °F

t_o — Cooling Water, Discharge Temperature, °F

rpm — Drum Rotary Speed

d — Drum Diameter, ft

l — Drum Width, ft

Secondary Variables:

R — f (L)(rpm)(d)(l) - Process Film Thickness

G — f $(T_i)(T_o)(L)(t_i)(t_o)$ - Cooling Water Rate

h — f $(rpm)(L)(T_i)(T_o)(l)$ - Depth of Drum Immersion

b — f (rpm) - Contact Time

MATHEMATICAL MODEL

The mathematical model chosen to describe the flaker operation is that of unidirectional unsteady state heat transfer in an infinite film layer. Figure 2 serves as an illustration. Since the temperature gradient in the X direction of heat transfer is usually 10^3-10^4 times that in the Z direction, and since ideally no temperature gradient exists in the Y direction, unidirectional transfer of heat is postulated to be a valid approximation for this case. In this model the process film layer with thickness R is exposed for a time interval, b, to the drum surface at temperature t. The amount of heat, Q_x, removed from the process film is a function of the film-drum contact time. Boundary conditions may be defined as follows:

At	b = 0	,	$T = T_i$
At	b = ∞	,	T = t
At	x = 0	,	T = t

The partial differential equation descriptive of the heat transfer mechanism depicted in Figure 2 is given in its general form in Equation (1).

$$\delta T/\delta b = (k/c\rho)\,\delta^2 T/\delta x^2 \tag{1}$$

- 5 -

The application of this equation to the flaking
process involves the validity of the following assumptions:

1. Negligible heat loss, process film to atmosphere.
(Experimentally shown not to exceed 15% of total heat transfer).

2. One hundred percent lateral drum coverage. (For
maximum utilization flakers are operated at >95% coverage).

3. Greater than ten ratio of d/R. (This ratio is in
the 10^4 range in plant operation).

4. Incremental removal of latent heat of solidification
in the X direction during the cooling process in the same
proportion as heat transfer across the interphase. (The film
temperature gradient insures this).

5. Approximately constant k within operational temper-
ature limits.

6. Approximately constant ratio of $(k/c\rho)$ within
operational temperature limits.

MATHEMATICAL SOLUTION

As indicated, assumptions 1-3 hold for most plant flaker
applications. Limiting the application of Equation 1 to chemical

process materials exhibiting physical properties within the limitations of assumptions 4-6, Equation 1 may then be solved by application of a Fourier Series expansion as previously demonstrated by Sherwood and Reed to yield Equation 2.[1] Thus for $(k/c\rho)(b)/R^2 \geqq 0.5$:

$$\ln E = \ln(8/\pi^2) - (\pi^2/4)(k/c\rho)(b/R^2) \qquad (2)$$

The expression E here represents the ratio of the sensible heat remaining in the flaked product above datum temperature t over all the heat removed in cooling to datum temperature t, i.e., an inverse measure of the cooling efficiency. Inclusion of the latent heat term follows assumption 4 :

$$E = (T_0 - t)\Big/(T_1 - t + \Delta H_s/c) \qquad (3)$$

The contact time b and film thickness R may, in Equation 2, be expressed in terms of primary operating variables as follows:

$$b = (0.0125)\text{rpm}^{-1} \qquad (4)$$

$$R = (5.3)(L)\Big/(\rho)(\text{rpm})(d)(1) \qquad (5)$$

Equation 4 predicates a drum circumferential film coverage of 270 degrees. The substitution of the primary

operating variables of Equation 4 and 5 into Equation 2 results in the general correlating equation defined by Equation 6.

$$\ln \left[\frac{T_0 - t}{T_1 - t + \Delta H_s/c} \right] = -0.21 - 1.092 \times 10^{-3} \left(\frac{k\rho}{c}\right)\left(\frac{rpm}{L^2}\right) (dl)^2 \qquad (6)$$

This expression demonstrates that the inverse of the cooling efficiency of a rotary drum cooler flaker is a logarithmic function of the drum rotary speed, the square of the drum area, and the inverse square of the processing rate. Processing stream physical properties are represented in the term $\left(\frac{k\rho}{c}\right)$ as affecting the cooling operation.

RESULTS

To test the validity of Equation 6, available flaker operational plant data were taken with a 48 in. x 28 in. (drum dimensions) flaker over a wide range of operating conditions. Upon insertion into Equation 6 the expected flake discharge temperature, T_0, was calculated. A comparison of these calculated values of T_0 to experimentally measured values showed a standard deviation of less than two percent. An example of the test information received with an arbitrary organic intermediate is shown in Table II.

TABLE II

APPLICATION OF EQUATION 6 TO ACTUAL OPERATING DATA

T_i °F	T_o °F	t °F	L M lb/hr	rpm	$\dfrac{T_o-t}{T_i-t+\Delta H_s/c}$	T_o by Eqn.6	$\pm$ % Error, T_o Calculated from T_o Experimental
342	219	139	3.04	11	0.267	225	+2.7
342	194	141	2.48	10 1/3	0.177	193	-0.5
342	193	141	2.45	10 1/3	0.174	192	-0.5
342	197	147	2.47	11	0.171	194	-1.5
341	195	140	2.47	10	0.184	197	+1.0
340	201	140	2.53	11	0.205	198	-1.5
340	172	143	1.65	6 1/3	0.099	175	+1.7
337	174	142	1.73	6 1/3	0.109	174	±0.0
342	166	146	1.56	6	0.068	167	+0.6
342	164	146	1.52	6	0.062	167	+1.8
345	155	146	1.13	4 1/2	0.030	154	-0.7

Figure 3 plots the data of Table II. The correlating equation shown was derived from Equation 6, by insertion of the corresponding drum dimensions of d = 48 in. and l = 28 in. and the physical properties of the organic intermediate.

Preliminary data received from tests with an additional 48 in. x 60 in. flaker unit further substantiated the excellent agreement of plant operational data with that predicted by Equation 6.

CONCLUSIONS

A mathematical expression was derived which effectively correlates rotary drum flaker design and operating variables for processing materials showing little change in thermal properties during cooling and solidification. The expression fits actual operating data within a standard deviation of two percent, based on flaker discharge temperature. Based on this excellent agreement, the expression should be useful as a basis for rotary drum cooler-flaker design and the choice of optimum operating conditions.

NOMENCLATURE

G	$=$	Coolant rate, lb/hr
ΔH_s	$=$	Latent heat of solidification, Btu/lb
L	$=$	Processing rate, Mlb/hr
R	$=$	Process film thickness, ft
T	$=$	Process film, average cross sectional temperature, °F
T_i	$=$	Process material, feed temperature, °F
T_o	$=$	Process material, discharge temperature, °F
b	$=$	Process film, drum surface contact time, hr
c	$=$	Process material heat capacity, Btu/lb/°F
d	$=$	Drum diameter, ft
h	$=$	Depth of drum immersion, ft
k	$=$	Process material thermal conductivity, Btu-ft/ft^2/°F/hr
l	$=$	Drum width, ft
t	$=$	Average coolant temperature, °F
t_i	$=$	Coolant inlet temperature, °F
t_o	$=$	Coolant exit temperature, °F
ρ	$=$	Process material density, lb/ft^3

REFERENCE

(1) Sherwood, T. K. and Reed, C. E. : "Applied Mathematics in Chemical Engineering," 1st Ed., p. 220, McGraw-Hill Book Company, Inc., 1939.
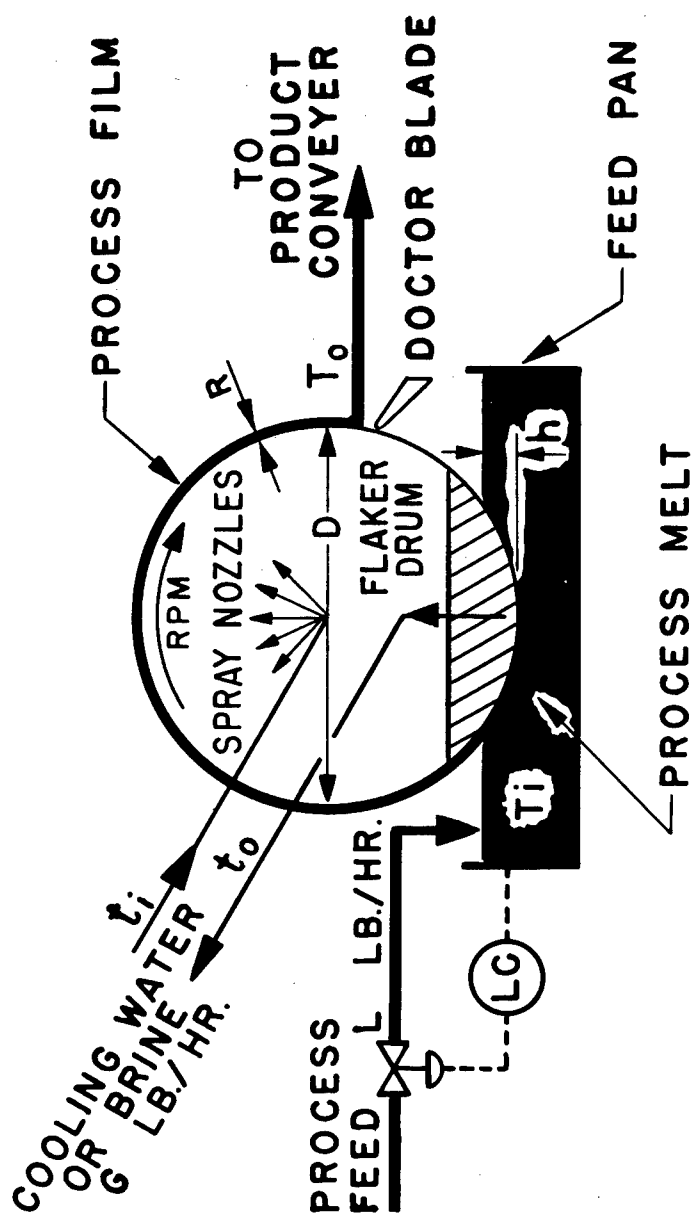
- 11 -

PROCESS FILM

TO PRODUCT CONVEYER

DOCTOR BLADE

FEED PAN

RPM

SPRAY NOZZLES

D

FLAKER DRUM

T_o

R

t_o

t_i

COOLING WATER OR BRINE G LB./HR.

PROCESS FEED L LB./HR.

LC

T_i

h

PROCESS MELT

FIGURE 1

ROTARY DRUM COOLER-FLAKER OPERATION

$Q_z = 0$

$Q_y \ll Q_x$

$Q_{atm} < Q_x$

Q_{atm}

PROCESS FILM

DRUM CASE

T_x

$X_{MAX} = R$

X

dx

t

Q_x

COOLING WATER

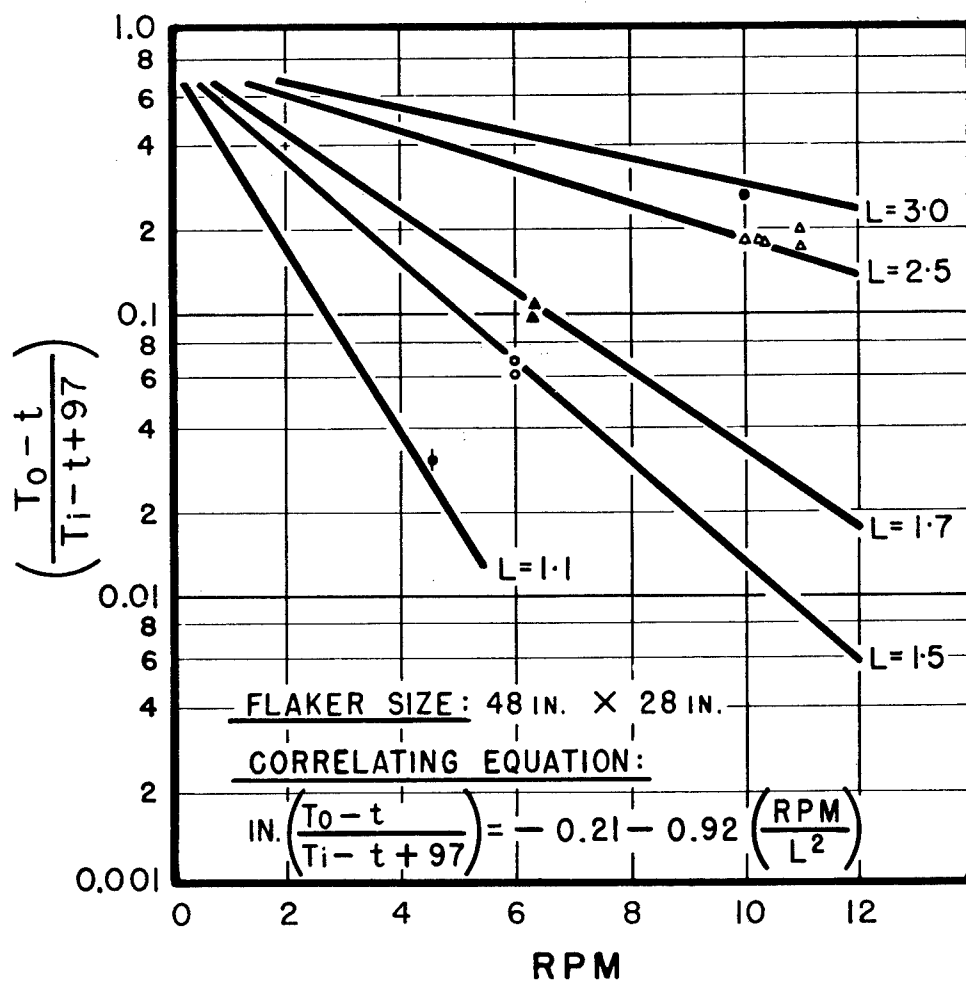FIGURE 2

FLAKER OPERATION - MATHEMATICAL MODEL

FIGURE 3

FLAKING OF ORGANIC INTERMEDIATE "A"
COMPARISON OF EXPERIMENTAL WITH PREDICTED DATA